

Adsorption Study of Lead Ions Pb²⁺ by Using Ion – Exchange Resin and Some Natural Clays

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Abstract

The adsorption capacity of three types of Iraqi clays (kaoline, porcelaine and bentonite) and three types of ion – exchange resin and imported zeolite are investigated. The adsorption data are presented using adsorption isotherm curves and are best fitted using the Langmuir adsorption equation that yields the maximum adsorption capacity of adsorbents (ion – exchange or clays). Iraqi clays show high adsorption capacity reached to 99.7% and sometimes similar to the adsorption capacity of ion – exchange. The effect of initial concentration of lead ions solutions on the amount of adsorption are studied also.

Langmuir constants equations have been calculated for the seven different adsorbate at 25°C. The percentage of lead removal at equilibrium increases with increasing initial lead ions concentrations. The results obtained could be useful for the application of Iraqi clays for the Pb²⁺ removal from industrial waste water.

Introduction

Lead is one of the most common toxic metals found at hazardous waste and superfund sites [1]. Sorption technology based on ion-exchange processes and physical and chemical sorption has found increasing application in various fields during the past years [2]. The use of sorption processes for the removal of heavy metals from waste water is especially promising. Inorganic sorbents are interesting because they are in many cases cheaper than polymeric chelate ion exchangers. However, sorption of heavy metals on inorganic sorbents depends strongly on the pH value and ion – exchange properties of the clay minerals [3-9]. The adsorption of Pb²⁺ by calcareous soil is poorly understood in contrast with adsorption by noncalcareous soils [10]. Most Iraqi studies related to Geological studies involved soil elements analyses and any mechanism adsorption study involving kinetics study about the objective of the present study is not found in searcher.

The adsorption reactions affects on mobility and availability of trace elements, including Pb. Adsorption isotherms most frequently used are Freundlich and Langmuir (i.e., equation (1) and (2), respectively)

$$Q = K_F C_e^n \quad \dots \dots \dots (1)$$

$$Q = (K_L b) / (1 + K_L C_e) \quad \dots \dots \dots (2)$$

Where; K_F and n are Freundlich coefficients; C_e is concentration of Pb²⁺ in equilibrium solution, mg L⁻¹; K_L is Langmuir coefficient related to binding energy of Pb to soil solids; and b is Langmuir adsorption maximum, i.e., the maximum amount of Pb adsorbed on soil solids as monolayer, mg/g; Q_s is the amount of Pb

adsorbed (mg/g) which calculated using the equation below:

$$Q = \frac{(C_0 - C_e)V}{m} \quad \dots \dots \dots (3)$$

Where; C₀ is the concentration of contaminant in the solution before mixing with adsorbent (mg/L); C_e is the equilibrium concentration of Pb left in the solution after the experiment (mg/L); V is volume of test solution (ml); and m is the mass of adsorbent.

The Langmuir Eq.2 can be rearranged into a linear form as shown in Eq.4 by plotting C_e/Q_s as a function of C_e. Parameters K_L and b can determined from the linear graph.

$$\frac{C_e}{Q_s} = \frac{1}{b} + \frac{K_L}{b} C_e \quad \dots \dots \dots (4)$$

The Langmuir model assumes that:

- (a) Adsorption energy is constant and independent of surface coverage;
- (b) Adsorption occurs at localized sites with no interaction between various ions in the solution;
- (c) Maximum adsorption occurs when the clay surface is covered by monolayer of cations.

Materials and Methods

The composition of Iraqi clays and Zeolite used in this study is given in Table 1, and the composition of the three standard ionic – exchanger is given in Table 2. (0.5 g) of clay sample or ionic – exchanger was placed with a solution was prepared by a suitable dilution of the standard lead acetate solution (concentration 1000 mg L⁻¹) with distilled water and all experiments were carried out in round bottom 250 ml. flasks at a constant temperature of 25°C using a rotary

shaker (100 rpm). A solution volume (100 mL) with different initial lead concentration and pH values was mixed with a definite amount of adsorbent.

After that the samples were shaken for (5, 10, 15, 20 and 30) min., the suspension was then filtered and the lead concentration in the filtrate was determined using atomic absorption spectroscopy (AAS) type GBC 993 plus (England) and the lead concentration (ppm) was determined.

The particle size of Iraqi clays were in the range of (50 - 5) μm while for Zeolite was 300 μm and for ionic-exchange range of (40 - 50) μm . The difference between the Pb concentration of initial solution and the filtered supernatant was taken as the Pb retained by the adsorbent surface.

Freundlich and Langmuir equation (1 and 4) were used to interpret the equilibrium adsorption data and respective adsorption coefficients were calculated. Stepwise regression procedure was used to study the relationship between the coefficients and the adsorbent properties.

Results and Discussions

The adsorption data show a highly significant fit to the Langmuir adsorption isotherm (Table 3). Adsorption isotherms were plotted between the amounts of lead ions adsorbed per gram of the clay sample (mg/g) as a function of the equilibrium free ion concentration in the solution (mg/L). Figures (1 - 7) show the amount of Pb adsorption by various clays, and Figures (8-14) show a linear relations of eq.4. The sequence of the variation of the maximum adsorption capacity (b) for the seven adsorbent at 10 mg/l lead ions was as:

$Z_2 < \text{Bentonite} < \text{Zeolite} < \text{Porceline} < Z_1 < \text{Kaoline} < Z_3$

At 20 mg/l lead ions the sequence was as:

$Z_2 < \text{Bentonite} < Z_3 < Z_1 < \text{Zeolite} < \text{Kaoline} < \text{Porceline}$

At 30 mg/l lead ions the sequence was as:

$Z_2 < \text{Bentonite} < Z_3 < Z_1 < \text{Kaoline} < \text{Zeolite} < \text{Porceline}$

At 40 mg/l lead ions the sequence was as:

$Z_2 < \text{Bentonite} < Z_1 < Z_3 < \text{Zeolite} < \text{Kaoline} < \text{Porceline}$

At 50 mg/l lead ions the sequence was as:

$Z_2 < Z_1 < \text{Zeolite} < \text{Bentonite} < Z_3 < \text{Kaoline} < \text{Porceline}$

In general porceline shows a highest maximum adsorption capacity (b), bentonite and kaoline show good maximum adsorption capacity reach to the ionic exchanger maximum capacity

values as shown in Table 3. The amount of adsorption of lead ions on the seven adsorbents surfaces increase with initial concentration of lead ions solution increase, because of the high adsorption capacity which calculated from Langmuir equation constant eq. (2). The Langmuir constant (K_L) which related to binding energy⁽¹¹⁾ of lead ions to clay surface were calculated also and the sequence of variation of (K_L) for various clay at 10 mg/l lead concentration was as:

$Z_2 < \text{Bentonite} < \text{Zeolite} < \text{Porceline} < Z_1 < \text{Kaoline} < Z_3$

At 20 mg/l concentration the sequence was as:

$Z_2 < \text{Bentonite} < Z_3 < Z_1 < \text{Zeolite} < \text{Kaoline} < \text{Porceline}$

At 30 mg/l concentration the sequence was as:

$Z_2 < \text{Bentonite} < Z_1 < Z_3 < \text{Zeolite} < \text{Kaoline} < \text{Porceline}$

At 40 mg/l concentration the sequence was as:

$Z_2 < Z_1 < \text{Bentonite} < Z_3 < \text{Zeolite} < \text{Kaoline} < \text{Porceline}$

And at 50 mg/l concentration the sequence was as:

$Z_2 < Z_1 < \text{Zeolite} < \text{Bentonite} < Z_3 < \text{Kaoline} < \text{Porceline}$

This results indicate to the existence of an active sites on Iraqi adsorbate (porceline, kaoline and bentonite), this active sites related with lead ions like ionic exchanger active sites (Z_3 , Z_1) and zeolite.

The Z_2 ionic exchanger show lowest efficiency reached to 53% only and show lowest adsorption capacity and K_L values which related to the variation of functional group as show in Table 2. Iraqi bentonite adsorbate removed 99.7% of lead ions which reach to the efficiency of Z_1 and Z_3 while Porceline and Kaoline removed (97 - 98)% of lead ions from the solution, table 4 shows the amount of adsorption and efficiency percentage of the seven adsorbent surfaces.

These preliminary results suggest that Iraqi clays seem to be important to the fixation of heavy metals, (i) the clays surface chemistry which determines properties like to the cation exchange capacity. (ii) The adsorption capacity of clays increase with initial concentration lead ions solution increased. Therefore, the knowledge of heavy metals retention by Iraqi clays are required.

Conclusion

The removal of lead ions from synthetic solution was demonstrated successfully on a laboratory scale with a selective ion - exchange process. The following conclusion can be drawn from this study:

The data obtained from this study applied to Langmuir and Freundlich isotherms.

The Langmuir isotherm gives an adequate correlation coefficient value (K_L , b). K_L indicate to the binding energy of lead ions to adsorbent surface; b indicate to the maximum amount of lead ions adsorbed on clay surface as monolayer.

Iraqi clays show high (K_L , b) values and adsorption efficiency reach to 99.7% (by using bentonite). The amount of adsorption of lead ions on the seven adsorbate surfaces increase with

initial concentration of lead ions increase. The mechanism of remove lead ions is ion - exchange with adsorbate active sites and physical adsorption and in the case of using bentonite, absorption processes was associated with adsorption processes, which resulted from the comparison between the maximum adsorption capacity of bentonite and the highest adsorption efficiencies 99.7% of lead ions adsorption.

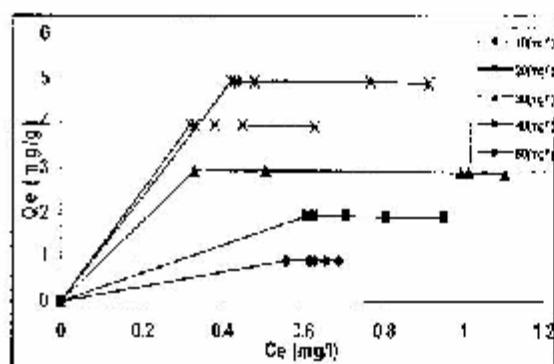


Fig 1: adsorption isotherms for (Z1).

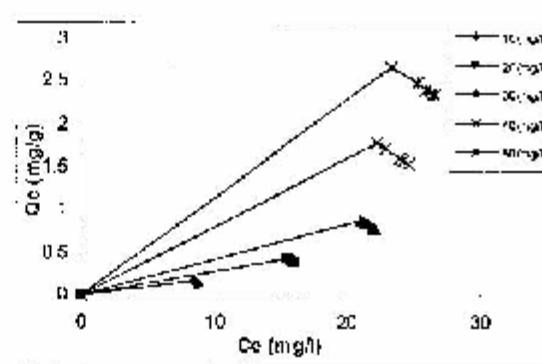


Fig 2: adsorption isotherms for (Z2).

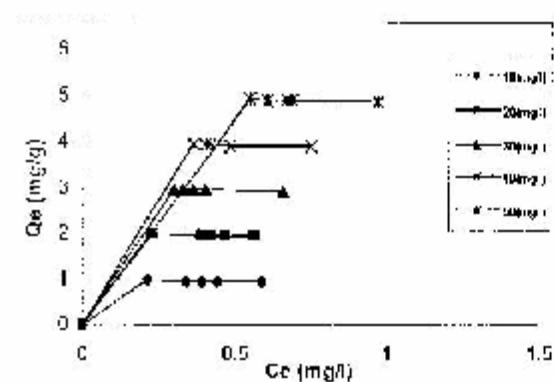


Fig 3: adsorption isotherms for (Z3).

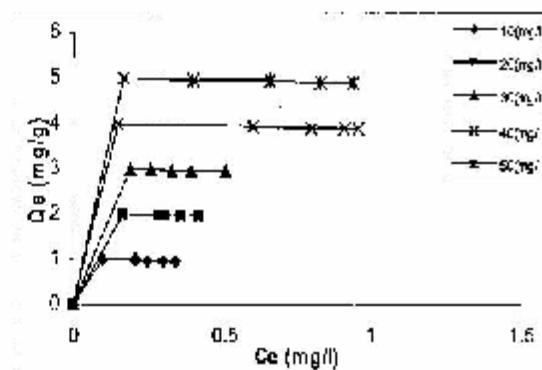


Fig 4: adsorption isotherms for Kaoline.

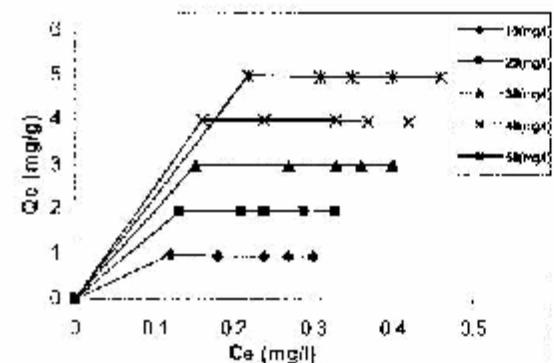


Fig 5: adsorption isotherms for Purceline.

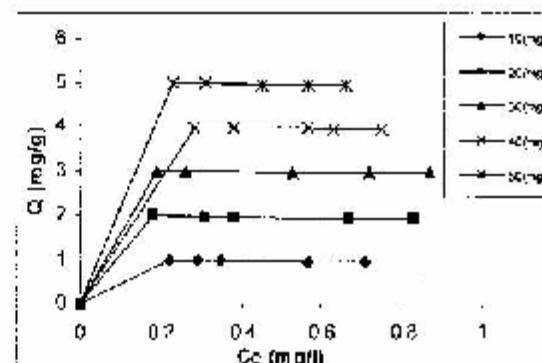


Fig 6: adsorption isotherms for Zeolite.

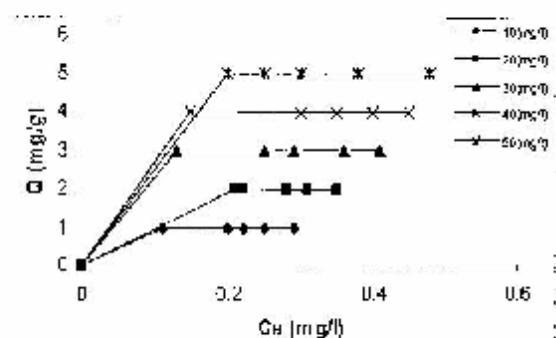


Fig 7: adsorption isotherms for Bentonite.

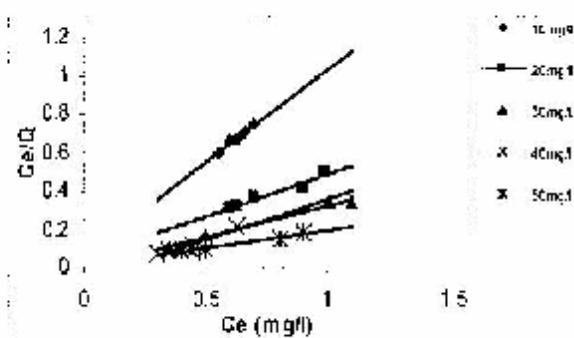


Fig 8: Linearised Langmuir isotherm for Z1

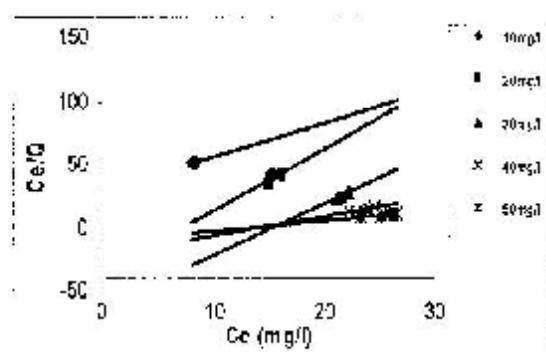


Fig 9: Linearised Langmuir isotherm for Z2

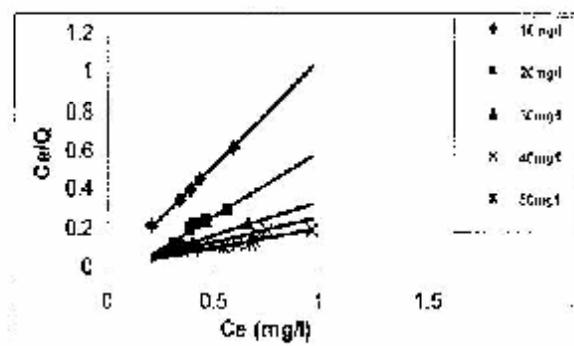


Fig 10: Linearised Langmuir isotherm for Z3

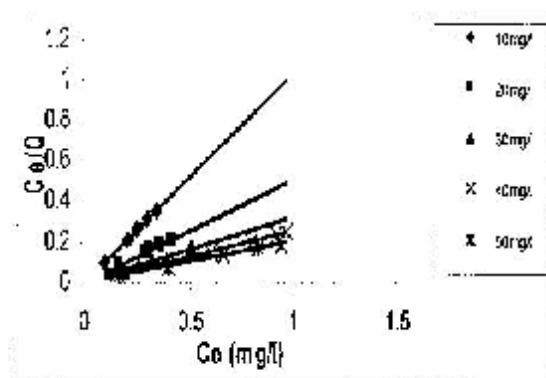


Fig 11: Linearised Langmuir isotherm for Kaoline

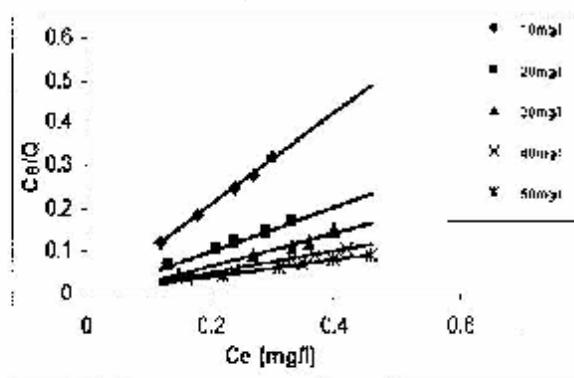


Fig 12: Linearised Langmuir isotherm for Porceline

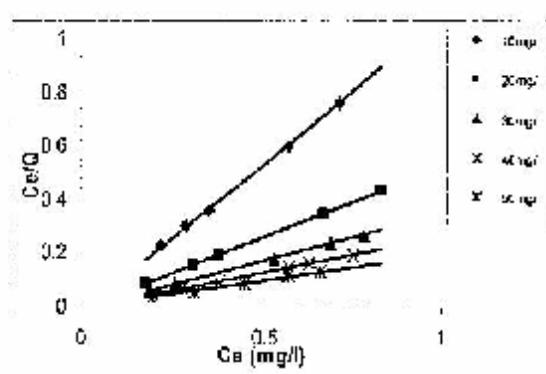


Fig 13: Linearised Langmuir isotherm for Zeolite

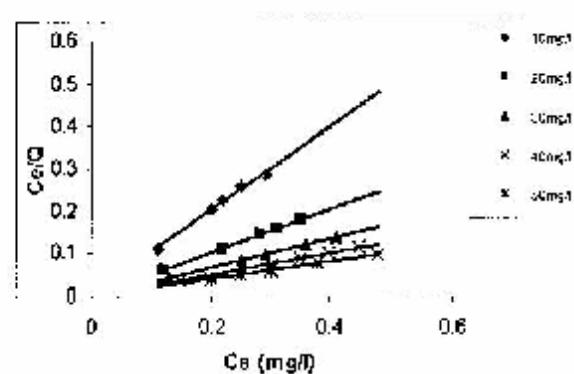


Fig 14: Linearised Langmuir isotherm for Bentonite

Table (1): chemical analyses of Iraqi clays (supplied geological scanning company)

Bentonite pH=7.63		Kaoline pH=7.66		Porceline pH=7.12		Zeolite pH=3.23	
Constituent	Wt.%	Constituent	Wt.%	Constituent	Wt.%	Constituent	Wt.%
SiO ₂	56.77	SiO ₂	48.57	SiO ₂	62.6	SiO ₂	32.52
Al ₂ O ₃	15.67	Al ₂ O ₃	35.05	Al ₂ O ₃	3.4	Al ₂ O ₃	27.64
CaO	4.48	CaO	0.6	CaO	8.1	CaO	11.38
MgO	3.42	MgO	0.77	MgO	6.3	Na ₂ O	4.20
K ₂ O	0.60	Na ₂ O	0.08	Na ₂ O	0.15	L.O.I.	24.25
Na ₂ O	1.11	Fe ₂ O ₃	1.34	Fe ₂ O ₃	1.2	—	—
Fe ₂ O ₃	5.12	TiO ₂	1.19	P ₂ O ₅	1.09	—	—
L.O.I.	12.49	L.O.I.	12	L.O.I.	14.1	—	—

Table (2): Properties of (Z₁, Z₂ and Z₃)

Z ₁			Z ₂			Z ₃		
Functional group	Water regain	Mesh	Functional group	Water regain	Mesh	Functional group	Water regain	Mesh
R-SO ₃ -H ⁺	0.3 - 0.15	52 - 100	R-CO ₂ -H ⁺	0.8 - 1.0	14 - 52	R-SO ₃ -H ⁺	0.46- 0.7	52 - 100

Table (3): Langmuir constant for adsorption Pb²⁺ on the seven surfaces.

Types of clays and resins	a					b				
	10	20	30	40	50	10	20	30	40	50
Z ₄	13.1869	7.8719	6.0714	6.6448	2.2453	13.755	18.18	18.867	15.576	11.11
Z ₂	0.1343	0.079	0.0648	0.0709	0.0814	0.003	0.0068	0.0157	0.0469	0.1029
Z ₁	68.2829	8.438	13.78	14.2819	8.5944	62.893	12.5156	40	55.55	14.66
Kaoline	25.4828	25.745	16.4	19.7692	20.46	24.3902	50	54	76.923	100
Porceline	9.9376	42.6179	38.06	42.1142	33.815	9.1743	83.3	100	166.66	166.66
Zeolite	5.4236	9.7536	17.21	17.0982	3.7882	4.9261	18.5185	50	66.66	19.607
Bentonite	1.8991	3.9376	4.8457	5.074	4.056	1.923	7.6923	14.285	20	20

Table (4) data of Ce, % and Q_e for adsorption lead ions on the seven surfaces.

Types of adsorbs hours	C _i (mg/l)	% of adsorption						% of desorption						Q _e (mg/g)							
		10	20	30	40	50	60	15	25	40	50	70	100								
Zn	0.56	0.61	0.35	0.32	0.42	1.5	1.50	91.16	96.53	98.9	99.2	99.16	99.25	99.7	0.044	1.937	2.367	3.968	4.938	19.88	40.45
Zn	8.35	15.6	21.22	22.2	32.2			16.20	21.92	29.03	44.5	53.6	—	—	0.162	0.419	0.890	1.720	2.63	—	—
Zn	0.21	0.23	0.30	0.36	0.25	1.4	1.70	97.90	98.83	99.00	99.1	98.95	99.30	99.6	0.979	1.917	2.970	3.964	4.845	19.86	49.01
Zn	0.10	0.17	0.19	0.15	0.17	40	55	97.00	98.15	99.35	99.6	99.65	99.60	99.6	0.960	1.982	2.931	3.983	4.588	15.60	36.30
Zn	0.12	0.13	0.13	0.16	0.22	20	150	98.8	99.25	99.50	99.6	99.55	99.60	99.6	0.998	1.987	2.985	3.964	4.578	18.00	37.50
ZnO	0.22	0.18	0.19	0.28	0.23	1.6	2.00	97.90	98.10	98.36	99.3	98.54	99.20	99.6	0.978	1.982	2.981	3.972	4.577	19.82	49.20
Ce	0.11	0.12	0.13	0.15	0.20	1.4	16.0	98.50	99.40	99.56	99.6	99.55	99.30	99.6	0.999	1.988	2.997	3.985	4.580	12.86	48.40

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الخلاصة

كانت دراسة سعة امتصار ٣٦٪ للزئاص من الأطيان العرجانية وهي (الكالوانين ، فلور سيراتن ، والبنتروذيل) وشلاط الزئاص من الراتنجات والنيزويولات المستورد . وتم تحليل النتائج لامتصار من خلال ايزوثيرمات الامتصار (منஸاوایک درجة الحرارة) والتي تطابقت مع مستويات لنكميلر المعروفة وبنها حصلنا على اعظم سعة امتصار لبراتنجات والأطيان العرجانية ونيزويولات . وظاهر أن للأطيان العرجانية سعة امتصار عالية وصلت إلى ٩٩.٧ % ، هذه التقرية مشابهة لسعة امتصار على الراتنجات ، كما ودرس تغير اخلاقف التركيز الأليكترانى لماء الأول يومات للرسان على كمية الامتصار (Oc) . وتم فحص ثبات معايير لنكميلر للمطروح الماء للسبعة عند درجة حرارة الغرفة (Oc25) ، إن نسبة ثبوت انساخى العزالة بـ الماء الماء للسبعة تزداد بزيادة التركيز الأليكترانى